Gas-liquid two phase flow through a vertical 90deg elbow bend


Published in:
Experimental Thermal and Fluid Science

Queen's University Belfast - Research Portal:
Link to publication record in Queen's University Belfast Research Portal

General rights
Copyright for the publications made accessible via the Queen's University Belfast Research Portal is retained by the author(s) and / or other copyright owners and it is a condition of accessing these publications that users recognise and abide by the legal requirements associated with these rights.

Take down policy
The Research Portal is Queen's institutional repository that provides access to Queen's research output. Every effort has been made to ensure that content in the Research Portal does not infringe any person's rights, or applicable UK laws. If you discover content in the Research Portal that you believe breaches copyright or violates any law, please contact openaccess@qub.ac.uk.
Gas–liquid two phase flow through a vertical 90° elbow bend

P.L. Spedding, E. Benard *

School of Aeronautical Engineering, Queen’s University Belfast, BT9 5AH, UK.

Received 24 March 2006; received in revised form 1 August 2006; accepted 7 August 2006

Abstract

Pressure drop data are reported for two phase air–water flow through a vertical to horizontal 90° elbow bend set in 0.026 m i.d. pipe. The pressure drop in the vertical inlet tangent showed some significant differences to that found for straight vertical pipe. This was caused by the elbow bend partially choking the inflow resulting in a build-up of pressure and liquid in the vertical inlet riser and differences in the structure of the flow regimes when compared to the straight vertical pipe. The horizontal outlet tangent by contrast gave data in general agreement with literature even to exhibiting a drag reduction region at low liquid rates and gas velocities between 1 and 2 m s⁻¹.

The elbow bend pressure drop was best correlated in terms of \( \frac{l_e}{d} \) determined using the actual pressure loss in the inlet vertical riser. The data showed a general increase with fluid rates that tapered off at high fluid rates and exhibited a negative pressure region at low rates. The latter was attributed to the flow being smoothly accommodated by the bend when it passed from slug flow in the riser to smooth stratified flow in the outlet tangent.

A general correlation was presented for the elbow bend pressure drop in terms of total Reynolds numbers. A modified Lockhart–Martinelli model gave prediction of the data.

Keywords: Air–water flow; Two phase flow in bend; Bend pressure loss; Prediction of pressure loss

1. Introduction

Single phase pressure drop can be predicted for curved pipes [1]. Recently Crawford et al. [2] extended the prediction ability to tight bends. Early work on two phase flow in curved pipes and bends highlighted difficulties in understanding the pressure drop characteristics [3–6]. Detailed studies of two phase pressure loss have largely been confined to the horizontal plane. Chenoweth and Martin [7] showed that while two phase pressure drop around bends is higher than for single phase flow it could be correlated by an adoption of the Lockhart–Martinelli [8] model developed originally for straight pipe. The correlation was claimed to predict loss in bends and other pipe fittings. Also at high mass velocities agreement was achieved with the homogeneous model. Fitzsimmons [9] presented two phase bend pressure loss data in terms of the equivalent length, \( l_e/d \) (i.e. the bend pressure loss over straight pipe frictional pressure gradient) and the Lockhart–Martinelli multiplier \( \phi_{LB} \) referred to the single phase gas pressure loss in the bend. Comparison against pressure drop in straight pipe gave a poor correlation. Sekoda et al. [10] also used \( \phi_{LB} \) referred to single phase liquid pressure loss in the bend. The two phase bend pressure drop was found to be independent of pipe diameter and depended on \( R/d \) in a manner similar to that found for single phase flow. Bruce [11] confirmed that the standard Lockhart–Martinelli parameter over-predicted bend pressure loss. Also the homogeneous model gave acceptable prediction of \( R_{12} \) refrigerant for bends presumably at high mass flows. Free-ston and Dole [12,13] presented widely scattered geothermal data. For long and short radius bends results were...
Nomenclature

$d$  pipe internal diameter, m
$G$  mass flow rate, kg m$^{-2}$s$^{-1}$
$L$  pipe length, m
$\ell_e$  equivalent length, m
$P$  pressure, kg m$^{-2}$s$^{-2}$
$Q$  volume flow rate, m$^3$s$^{-1}$
$R_e$  Reynolds number, d$\overline{V}$/$\mu$
$U^*$  shear velocity, m s$^{-1}$
$\overline{V}$  velocity, m s$^{-1}$
$W$  mass flow rate, kg s$^{-1}$
$X$  Lockhart–Martinelli parameter, Eq. (4)
$X, Y, Z$  inlet pipe, bend, outlet pipe, length, m.
$\rho$  density, kg m$^{-3}$
$\mu$  viscosity, kg m$^{-1}$s$^{-1}$
$\phi$  Lockhart–Martinelli pressure parameter

Subscripts

A  total mass as liquid
B  bend
E  equivalent
f  friction
G  gas
L  liquid
P  phase
S  superficial
T  total
X  fluid

53 $R/d = 90$, $\ell_d/\ell = 225$ [±20%]; $R/d = 1.5$, $\ell_d/\ell = 58$ [±30% to $–40\%]$; T, $\ell_d/\ell = 115$ [±50% to $–75\%$]. Despite wide variation of the data it was used by the Engineering Science Data Unit [14] to develop a model for two phase flow through pipe components. Chisholm [15] presented an elementary model for prediction of two phase flow in bends, based on $\phi_{1/4}$, which was claimed to give prediction for all pipe diameters, $R/d$ values and flow rates. Noersteboe [16] showed the model gave high values of bend pressure loss when checked against refrigerant data. Most studies have taken little interest in the actual flow regimes present. In some cases they are mentioned only in passing. However, Hoang and Davies [17] have realised the significance of flow regimes and have reported data on bubbly flow in vertical return bends. Graf and Neti [18] studied two phase pressure drop in square bends. Reported work on the orientation of the plane of the bend has often given contrary results. Deobold [19] claimed that the horizontal bend, the horizontal to vertical up bend and the vertical down to horizontal bend all gave the same bend pressure loss. However a horizontal to vertical down bend had a pressure drop that was 35% less. The correlation for elevation was assumed to follow the homogeneous model by Deobold [19] but others such as Alves [20] ignored head pressure differences entirely. Peshkin [21] reported that horizontal to vertical down flow had about 10% more bend pressure drop than the corresponding horizontal to vertical up flow case. Kutateladze [22] by contrast concluded the direct opposite that the horizontal to vertical up flow bend created the greater pressure drop. Pressure drop in geothermal expansion loops also reported some contrary results [23–25]. Studies in helical coils and boilers have been conducted [26–33]. Modelling of the pressure drop data have been attempted with the Lockhart–Martinelli parameter [8] or the Baroczy [34] model [32,33]. Hart et al. [30] also developed models for low liquid flows. Rippel et al. [31] showed that the bend pressure loss varied significantly with the flow regime present. Work has recently been presented on water hammer in bends [35].

It can be concluded that a two phase flow through a curved pipe and elbow bends possesses similar features to those for a single phase flow. It is not clear as to the best method of data presentation and modelling, while the effects of flow regimes on the pressure drop which must be of significance requires elucidation. Currently uncertainties have been handled by over design. Such an approach is suspect particularly where safety issues are involved. For example, conveying to a destructor unit of the sudden release from safety valves where unexpected back pressure could be a real hazard.

In this work two phase air water flow through a vertical 90° to horizontal elbow bend is investigated.

2. Experimental

The apparatus of diameter = 0.026 m pipe is shown schematically in Fig. 1 together with details of the elbow bend. Air and water were fed into the base of the vertical riser and could be a real hazard. The apparatus of diameter = 0.026 m pipe is shown schematically in Fig. 1 together with details of the elbow bend. Air and water were fed into the base of the vertical riser and were manipulated. A cyclone separator detached the outgoing liquid for recirculation without back pressure effects. Tapping points, with separation cups attached, were used to measure the pressure loss (using a Solomat Zephyr manometer with ±1% accuracy) over three sections of the apparatus; the inlet vertical tangent leg $X$, the elbow bend region $Y$ and the outlet horizontal tangent leg $Z$. Additional tapping points set at 0.1 m intervals were also placed at points along the inlet and outlet legs. These were used to determine the bounds of the regions, $X$, $Y$ and $Z$ and were blocked during data collection. Holdup valves were located in sections $X$ and $Z$. Preliminary experiments were con-
ducted using the full range of flow rates with and without
the elbow bend in place to determine pressure gradients
etc so as to ensure the settling down lengths used were
adequate. With the elbow bend in place preliminary
experiments were conducted to determine the pressure
profiles across the apparatus (Fig. 2 is an example) and to
ensure a linear pressure gradient in regions X and Z so as
to allow accurate extrapolation into region Y. The pressure
at the base of the inlet leg varied up to \(1.35 \times 10^5\) kg m\(^{-1}\) s\(^{-2}\)
(a). Single phase experiments were also performed. Further
details of the apparatus and method used are given by
Woods and Spedding [36].

---

3. Results

In two phase vertical to horizontal flow the conditions in
the tangent legs either side of the elbow bend (in the regions
X and Z of Fig. 1) will be dramatically different since the
effects of gravity and uplift forces in the inlet vertical
tangent leg X will be absent in the outlet horizontal tangent
leg Z. Secondly, often the flow regimes and other flow
phenomena will be different in the two tangents. Therefore,
the calculation of the pressure drop over the elbow bend
will be more complex than that for single phase flow where
the phase density is essentially constant and the straight
pipes frictional pressure loss can be used to calculate elbow
drop pressure loss regardless of the orientation of the plane
of the bend. This was not the case for two phase flow where
the total pressure drop in each tangent must be used in the
calculation as detailed in Fig. 2. In the figure A–C and D–F
are the actual up and downstream pipe tangent lengths, C–
D is the elbow bend total centre line length, B–C and D–E
are the up and downstream transitional regions. The point
G is the demarcation between the straight pipe pressure
drop of the two tangents which was chosen, not half way
at the 45° line but at the 90° intersection where gravity
effects in the vertical tangent cease. This was done because,
in general the pressure loss in the vertical tangent X was
orders of magnitude greater than the corresponding hori-
zontal tangent Z pressure drop. The actual pressure distri-
bution in Fig. 2 is abcdef, while the straight pipe
distribution in the two tangent legs are abc'g' and g'd'e'f'.
The corrected pressure distribution abc'g''d''e''f'' includes
a straight pipe loss equal to the actual length C–D of the
elbow bend centre line, \(\Delta P_{BE}\), that is composed of C–G

---

Please cite this article as: P.L. Spedding, E. Benard, Gas–liquid two phase flow through a vertical 90° elbow bend, Experimental Ther-
mal and Fluid Science (2006), doi:10.1016/j.expthermflusci.2006.08.003
169 and G–D the two elements from each tangent leg. Thus the
170 total bend pressure drop $\Delta P_{BT}$ is composed of the bend
171 pressure loss from the inlet and outlet tangent legs pressure
172 gradients $\Delta P_B$ and the equivalent centre line bend length
173 $\Delta P_{BE}$ (see Table 1).
174 In the calculation of $\Delta P_{BT}$ it was assumed that the
175 actual pressure drops in the vertical $X$ and horizontal $Z$
176 tangents should be used to determine $\Delta P_{BE}$. While the
177 latter should not cause any problems the former pressure
178 drop may be different to that in a straight vertical pipe
179 due, in the main, to increased liquid holdup. Therefore, possible distur-
180 bances due to the elbow bend resulting in a narrower but increased fre-
181 quency of pressure fluctuations. In addition, the liquid
182 holdup tended to be higher with the elbow bend which,
183 particularly at the higher liquid rates, led to the head pres-
184 sure loss was larger with the inclusion of the elbow bend,
185 across the entire gas range. In the regions where the pres-
186 sure loss was the same for both systems. At low gas rates about
187 $G_{SG} = 0.8–1.5 \text{ kg m}^{-2} \text{s}^{-1}$ the frictional pressure drop
188 (being the total minus the head) gave a negative value. As the liquid rate was increased from Figs. 3–6 a difference
189 between the total pressure loss between the two systems
190 began to appear which eventually extended progressively
191 across the entire gas range. In the regions where the pres-
192 sure loss was larger with the inclusion of the elbow bend,
193 the flow regimes between the two systems exhibited subtle
194 differences, e.g. the slugs tended to be of shorter length with
195 the elbow bend resulting in a narrower but increased fre-
196 quency of pressure fluctuations. In addition, the liquid
197 holdup tended to be higher with the elbow bend which,
198 particularly at the higher liquid rates, led to the head pressure
199 loss with the elbow bend being above that of the
200 straight vertical pipe. Indeed the head pressure loss exhibited
201 a more marked effect with increasing gas rate than the
202 total head loss. The effect of uplift was less noticeable with
203
204 Table 1
205 Two phase flow in curved pipe and bends
206
<table>
<thead>
<tr>
<th>Fluids</th>
<th>Diameter</th>
<th>$R/a$</th>
<th>Geometry</th>
<th>Flow</th>
<th>Correlation</th>
<th>Ref.</th>
</tr>
</thead>
<tbody>
<tr>
<td>Air–water</td>
<td>0.0780</td>
<td>7.5</td>
<td>180° bend</td>
<td>Horizontal</td>
<td>$\phi^2_{LA}$ against $Q_l/Q_T$</td>
<td>[7]</td>
</tr>
<tr>
<td>Steam–water</td>
<td>0.0488</td>
<td>1.5, 5.2</td>
<td>90° bend</td>
<td>Horizontal</td>
<td>$\phi^2_{GB}$ against $l/d$</td>
<td>[9]</td>
</tr>
<tr>
<td>Air–water</td>
<td>0.018, 0.0257</td>
<td>2.36, 5.02</td>
<td>90° bend</td>
<td>Horizontal</td>
<td>$\phi^2_{LB}$</td>
<td>[10]</td>
</tr>
<tr>
<td>Air–water</td>
<td>0.019</td>
<td>4.6, 10.5, 14.5, 22.6</td>
<td>90° bend</td>
<td>Horizontal</td>
<td>$\phi^2_{LB}$</td>
<td>[11]</td>
</tr>
<tr>
<td>Air–water</td>
<td>0.019</td>
<td>1, 2, 3, 4, 5, 6</td>
<td>90° bend</td>
<td>Horizontal</td>
<td>$l/d$ against $\tau_L$</td>
<td>[11]</td>
</tr>
<tr>
<td>Steam–water</td>
<td>0.01</td>
<td>0.75, 4.5</td>
<td>90°, 45°, 180° bends</td>
<td>Horizontal</td>
<td>$\Delta P_{TP} = \Delta P_{LA}/\Delta P_{GA} - \Delta P_{LA}$</td>
<td>[12]</td>
</tr>
<tr>
<td>$R_{12}$, $R_{177}$</td>
<td>0.0223, 0.0825, 0.120</td>
<td>1.3, 1.4</td>
<td>90°, 180° bends</td>
<td>Horizontal</td>
<td>$l/d$ against $R_{SG}$</td>
<td>[20]</td>
</tr>
<tr>
<td>Air–water</td>
<td>0.0266</td>
<td>7</td>
<td>180° bend</td>
<td>Horizontal to vertical</td>
<td>$l/d$ against $R_{SG}$</td>
<td>[20]</td>
</tr>
<tr>
<td>Air–oil</td>
<td>0.0266</td>
<td>1.5</td>
<td>90° bends in vertical square coil</td>
<td>Horizontal, up and down vertical</td>
<td>$\phi^2_L$</td>
<td>[19]</td>
</tr>
<tr>
<td>Steam–water</td>
<td>0.307</td>
<td>1.5</td>
<td>90° bends in expansion loop</td>
<td>Horizontal to up and down vertical</td>
<td>$\phi^2_L$</td>
<td>[23]</td>
</tr>
<tr>
<td>Steam–water</td>
<td>0.201</td>
<td>1.5</td>
<td>90° bends</td>
<td>Up, down vertical to horizontal</td>
<td>$\phi^2_{LG}$ against $W_{SL}/W_{L}$</td>
<td>[24]</td>
</tr>
<tr>
<td>Air–water</td>
<td>0.0102</td>
<td>9.95</td>
<td>Up right helical</td>
<td>Down</td>
<td>$\phi^2_G$</td>
<td>[31]</td>
</tr>
<tr>
<td>Freon 12–water</td>
<td>0.0159</td>
<td>4.8, 7.2, 9.6</td>
<td>Up right helical</td>
<td>Up</td>
<td>Film inversion</td>
<td>[27]</td>
</tr>
<tr>
<td>Air–2/propanol</td>
<td>0.0127</td>
<td>22.8, 52.0, 92.9, 101.6</td>
<td>Up right helical</td>
<td>Up</td>
<td>$\phi^2_{LA}$</td>
<td>[32]</td>
</tr>
<tr>
<td>Air–water</td>
<td>0.0147</td>
<td>14.4</td>
<td>Up right helical</td>
<td>Up</td>
<td>$\tau_L$</td>
<td>[33]</td>
</tr>
<tr>
<td>Air–aq glycerol</td>
<td>0.0254</td>
<td>1, 5, 10</td>
<td>30°, 45°, 60°, 90°</td>
<td>Up</td>
<td>Data</td>
<td>[28]</td>
</tr>
<tr>
<td>Air–water</td>
<td>0.0254</td>
<td>12</td>
<td>180° vertical</td>
<td>Up/down</td>
<td>Data</td>
<td>[29]</td>
</tr>
</tbody>
</table>

Please cite this article as: P.L. Spedding, E. Benard, Gas–liquid two phase flow through a vertical 90° elbow bend, Experimental Thermal and Fluid Science (2006), doi:10.1016/j.expthermflusci.2006.08.003
the elbow bend in place and the frictional loss was virtually unaltered from that of the straight vertical pipe. Thus the inclusion of the elbow bend gave a similar effect to that noted by Spedding et al. [37], for the case when the pipe was slightly off the vertical where the anisotropy of the liquid flow caused an increase in both liquid holdup and pressure drop over vertical pipe under similar conditions. In addition the elbow bend caused an increase in the absolute pressure within the inlet vertical tangent leg \( X \) due to a measure of throttling of the flow by the elbow bend. Thus the presence of the elbow bend often led to an increase in the absolute pressure within the inlet vertical tangent leg \( X \) due to a measure of throttling of the flow by the elbow bend. This Fig. 3. Pressure drop in the vertical riser leading to the elbow bend compared to straight vertical pipe flow. \( G_{SL} = 10.97 \text{ kg m}^{-2} \text{s}^{-1}, \) \( d = 0.026 \text{ m i.d.} \) Frictional pressure drop, total pressure loss minus head pressure drop calculated from holdup. Fig. 4. Pressure drop in the vertical riser leading to the elbow bend compared to straight vertical pipe flow. \( G_{SL} = 62.67 \text{ kg m}^{-2} \text{s}^{-1}, \) \( d = 0.026 \text{ m i.d.} \) Frictional pressure drop, total pressure loss minus head pressure drop calculated from holdup. gas rates \( \bar{V}_{SG} = 1.5-2.5 \text{ m s}^{-1} \) there was a region of drag reduction where \( \frac{\Delta P_{BT}}{\Delta P_{SG}} = \phi_G < 1.0. \) This was in agreement with the findings of Ferguson and Spedding [43] who reported on this phenomenon in two phase horizontal flow in pipes with a size range of 0.045–0.051 m i.d. This work shows that the effect appeared at the lower diameter of 0.026 m as well. Fig. 8 gives the total elbow bend pressure drop \( \Delta P_{BT} \) for four liquid rates. At the lower liquid rates, the elbow bend positive pressure drop passed through a slight minimum value as \( \bar{V}_{SL} \) was increased. As the liquid rate increased the pressure drop rose steadily with \( \bar{V}_{SG} \) and possessed very few other features. There was an observable difference between the pressure drop relation that depended on whether \( \bar{V}_{SL} \) was below or above the free bubble rise velocity in the inlet vertical tangent leg \( X \). At the lower liquid (and gas rates) the elbow bend pressure drop was negative while at the highest liquid (and gas rate) the pressure drop commenced to level off. These observed effects can be attributed to the flow regimes present in the two tangent legs of the elbow bend. The negative elbow bend pressure drop region at the lower phase flow rates occurred when the slug regime in the inlet vertical tangent leg \( X \) passed smoothly through the elbow bend and formed the smooth stratified regime in the outlet following the method of Spedding et al. [42]. One interesting feature in Fig. 7 was that at low liquid velocities and
horizontal tangent leg Z. As the liquid (and gas) rate was increased the regime in the outlet horizontal tangent leg Z became successively stratified plus roll wave flow and stratified blow through slug and the negative pressure loss region passed since there was no longer a smooth regime transition within the elbow bend. The pressure drop tended to level off when the flow regime in the inlet vertical tangent leg X passed from churn to semi-annular flow. A slight minimum in the pressure drop relation occurred when the flow regime in the outlet Z passed from stratified roll wave to either annular roll wave or film plus droplet flow. When the liquid velocity in the inlet vertical tangent leg X exceeded the Taylor bubble rise velocity at low gas rates the slug or blow through slug regimes initially occurred in the outlet Z and the elbow bend pressure drop relation against $\overline{F}_{SG}$ tended to be rather flat. When the regimes changed to stratified roll wave as the gas rate was increased, the elbow bend pressure loss started to rise. In this region the elbow bend commenced to act as a droplet generator causing the pressure loss to rise rapidly.

Because of the low $R/d$ value of the elbow bend used in this work, the contribution of $\Delta P_{BT}$ to the total elbow bend pressure drop $\Delta P_{BT}$ was only a few percent, but flow regimes present in the tangent leg had a considerable effect on $\Delta P_{HT}$. When the elbow bend pressure loss $\Delta P_{BT}$ was expressed as $l_e/d$, using the actual pressure drop in the inlet vertical tangent leg $X$ for the calculation of the equivalent pipe length $l_e$, the data drew closer together and exhibited a general upward rising trend as shown in Fig. 9. The only regions not following the general trend were at the low phase flow conditions where negative pressure drops were in evidence and the highest phase flow conditions where the pressure drop tended towards a $l_e/d$ value of about 37.

The data did not exhibit a regular relationship if other pipe friction values were used such as the straight vertical pipe or outlet pressure drops. The same was true when other correlating parameters such as $W_G/W_L$ or $V_L$ were employed. This observation adds weight to those made by a number of workers and mentioned earlier that a better correlation of the Lockhart–Martinelli type was obtained if the single phase pressure loss used in the correlation referred to that actually obtained through the bend and not in straight pipe.

The data in Fig. 9 was correlated by

$$l_e/d = 0.001384Re_T - 13.53 \quad (2)$$

for the elbow bend pressure drop for two phase gas–liquid flow through a vertical upwards to horizontal $R/d = 0.6539$ bend over the ranges of positive $l_e/d$ values from $Re_{SG} = 2000–30,000$ and $Re_{SL} = 280–9800$. Over these ranges of...
Reynolds numbers the accuracy of prediction was with 1% average (range +56% to −38%).

Fig. 10 shows the data of this work plotted after the Lockhart–Martinelli [8] model as suggested by Fitzsimmons [9] and Sekoda et al. [10].

\[
\phi_s = \left[ \frac{\Delta P_{TP}}{\Delta P_{SX}} \right]_B
\]

\[
X = \left[ \frac{\Delta P_{SL}}{\Delta P_{SG}} \right]_B
\]

These data follow a consistent pattern only when expressed in terms of the single phase pressure loss in the bend. The use of other pressure drops such as that in the riser tangent or outlet horizontal tangent did not present a logical picture. The data obtained here do not follow the results of either Fitzsimmons [9] or Sekoda et al. [10], neither do they show agreement with the ESD [14] model, the elementary model of Chisholm [15] or the homogeneous model mentioned by Chenoweth and Martin [7], but suggest that the plane of the bend had an important influence on the elbow bend pressure loss. Data from Sekoda et al. [10] are given to illustrate the difference between this work.

4. Conclusions

The pressure loss in the inlet vertical tangent leg \(X\) showed significant differences to that for the straight vertical pipe, particularly at the higher fluid flow rates. This was caused by the following elbow bend providing some measure of choking of the flow that resulted in a build-up of pressure and liquid in the inlet vertical tangent leg \(X\) when compared to the straight vertical pipe.

The outlet horizontal tangent leg \(Z\) gave pressure loss results that were in agreement with reported data. A drag reduction region was shown to exist for the lower liquid flow rates under 0.07 m s\(^{-1}\) and gas flows of 1–2 m s\(^{-1}\).

The elbow bend pressure loss also exhibited a negative pressure loss regime at low fluid flow rates. The effect was attributed to the smooth conversion by the elbow bend of the slug flow in the inlet vertical tangent leg \(X\) to smooth stratified flow in the outlet horizontal tangent leg \(Z\).

A general correlation was presented for the elbow bend pressure drop in terms of the total Reynolds numbers. It was shown that the elbow bend pressure loss was best handled in terms of \(l/d\) calculated using the actual pressure loss in the inlet vertical tangent leg \(X\). Further the Lockhart–Martinelli bend parameters gave a useful method of presenting the data.
Fig. 8. Total elbow bend pressure drop against $V_{SG}$ for various liquid rates.

Fig. 9. Elbow bend pressure drop as $l/d$ against $Re_{SG}$.

Fig. 10. Elbow bend pressure drop according to the Lockhart–Martinelli model. $d = 0.018 - R/d = 2.36, 5.02$ [10].

Please cite this article as: P.L. Spedding, E. Benard, Gas–liquid two phase flow through a vertical 90° elbow bend, Experimental Thermal and Fluid Science (2006), doi:10.1016/j.expthermflusci.2006.08.003
References


